



EUROPEAN CENTRE FOR RESEARCH AND ADVANCED TRAINING IN SCIENTIFIC COMPUTING



Cantera



## Special features of cantera-avbp



## Several features are coded in cantera-avbp

1. AVBP transport model
2. The use of custom kinetics
3. Thickening a flame
4. Alternative remeshing possible
5. Partial Equilibrium Assumption for 2S chemistry
6. Flamelet computation
7. Soot equations

# 1. Transport

What are we talking about ?

- $D$  : Diffusion coefficient [ $\text{m}^2/\text{s}$ ]
- $\lambda$  : Thermal conductivity [ $\text{J}/\text{K}/\text{m}^3$ ]
- $\mu$  : dynamic viscosity [ $\text{Pa}\cdot\text{s}$ ]

$$\left\{ \begin{array}{l} \rho = \frac{p\bar{W}}{RT} \\ \rho \frac{\partial V}{\partial t} + \rho u \frac{\partial V}{\partial z} + \rho V^2 = \frac{\partial}{\partial z} \left( \mu \frac{\partial V}{\partial z} \right) - \lambda \\ \rho \frac{\partial Y_k}{\partial t} + \rho u \frac{\partial Y_k}{\partial z} = - \frac{\partial j_{k,z}}{\partial z} + \omega W_k \\ \rho C_p \frac{\partial T}{\partial t} + \rho u C_p \frac{\partial T}{\partial z} = \frac{\partial}{\partial z} \left( \lambda \frac{\partial T}{\partial z} \right) - \sum_{k=1}^K C_{pk} j_{k,z} \frac{\partial T}{\partial z} - \sum_{k=1}^K h_k \omega_k W_k \end{array} \right.$$



# 1. Transport

You have anyway in cantera, based on Lennard-Jones potentials :

- For the viscosity :

$$\mu_k = \frac{5}{16} \frac{\sqrt{\pi m_k k_B T}}{\pi \sigma_k^2 \Omega^{(2,2)*}}$$

- $m_k$  : the mass of species k
- $\sigma_k$  : the collision diameter of species k
- $T$  : temperature of the mixture
- $\Omega^{(2,2)*}$  : collision integral

$$\mu = \sum_k \frac{X_k \mu_k}{\sum_j X_j \phi_{kj}} \quad - \quad \phi_{kj} = \frac{1}{\sqrt{8}} \left(1 + \frac{W_k}{W_j}\right)^{-\frac{1}{2}} \left(1 + \left(\frac{\mu_k}{\mu_j}\right)^{-\frac{1}{2}} \left(\frac{W_j}{W_k}\right)^{\frac{1}{4}}\right)^2$$

- For the heat conductivity :

$$\lambda_k = \frac{\mu_k}{W_k} (f_{trans} C_{v,trans} + f_{rot} C_{v,rot} + f_{vib} C_{v,vib})$$

$$\lambda = \frac{1}{2} \left( \sum_k X_k \lambda_k + \frac{1}{\sum_k X_k / \lambda_k} \right)$$

<https://www.cerfacs.fr/avbp7x/HELP/MOULINETTE/XML2AV/xml2av.pdf>

# 1. Transport

- For the diffusion :

## 1. Multi

Inverse a diffusion matrix to each coefficient  $D_{jk}$ .

Best in terms of accuracy.  
Very very long !!

```
gas.transport_model = 'Multi'
```

Or 

```
transport = 'Multi'
```

 in the .cti

## 2. Mix

$$D_{jk} = \frac{3}{16} \frac{\sqrt{2\pi k_B^3 T^3 / m_{jk}}}{p\pi\sigma_{jk}^2 \Omega^{(1,1)*}}$$

- p : pressure
- $m_{jk}$  : reduced molecular mass  $m_{jk} = (m_j m_k) / (m_j + m_k)$
- $\sigma_k$  : the collision diameter of species k
- T : temperature of the mixture
- $\Omega^{(1,1)*}$  : collision integral

$$D_{km} = \frac{1 - Y_k}{\sum_{j \neq k} X_j / D_{jk}}$$

Best in terms of accuracy/cost.  
Still costly if used in 3D codes.

```
gas.transport_model = 'Mix'
```



# 1. Transport

3. Lewis ( $Le_k = \frac{Sc_k}{Pr} = 1$ )

Very low cost.

Big loss in accuracy !

**Simplified expression**

$$D_{km} = \frac{\lambda}{\rho C_p}$$

`gas.transport_model = 'UnityLewis'`

# 1. Transport

## 4. AVBP ( $Le_k = c^{te}$ )

Low cost.

Loss in accuracy, you have to check !

**Power law**      or

$$\mu = \mu_0 \left( \frac{T}{T_0} \right)^\beta$$

**Sutherland law**

$$\mu = \mu_0 \left( \frac{T}{T_0} \right)^{3/2} \frac{T_0 + S}{T + S}$$

**Simplified expression from  $Sc_k$**

$$D_k = \frac{\mu}{\rho Sc_k}$$

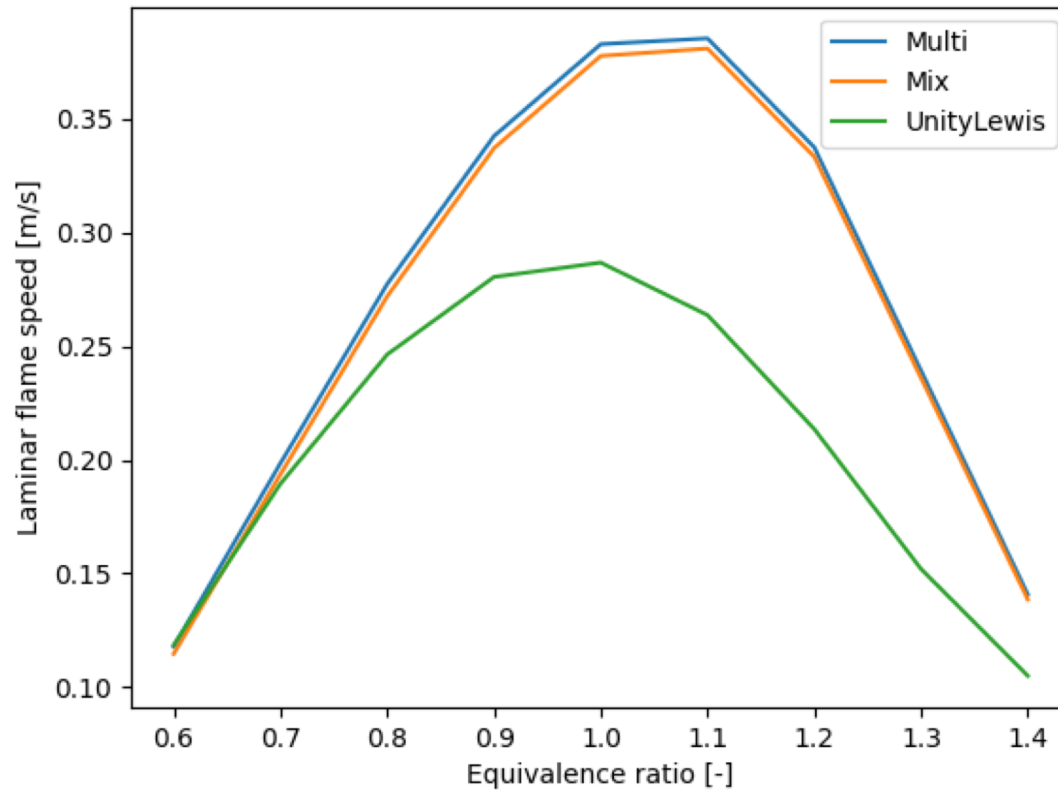
**Simplified expression from  $Pr$**

$$\lambda = \frac{C_p \mu}{Pr}$$

`gas.transport_model = 'AVBP'`

# 1. Transport

Gri 30 with  $T=300\text{K}$ ,  $P=1\text{bar}$ .







## 2. *Customkinetics*

If you want to give another thing to CANTERA than the information provided in a .cti.

- A f90 to be included in the code
- Useful if you want to have a special handling of the kinetics (ex: algebraic relations between species)

`kinetics = 'custom'` in the .cti

```
import cantera as ct
ct.compile_fortran('mechanism.f90')
```

in the script

# 3. Thickening

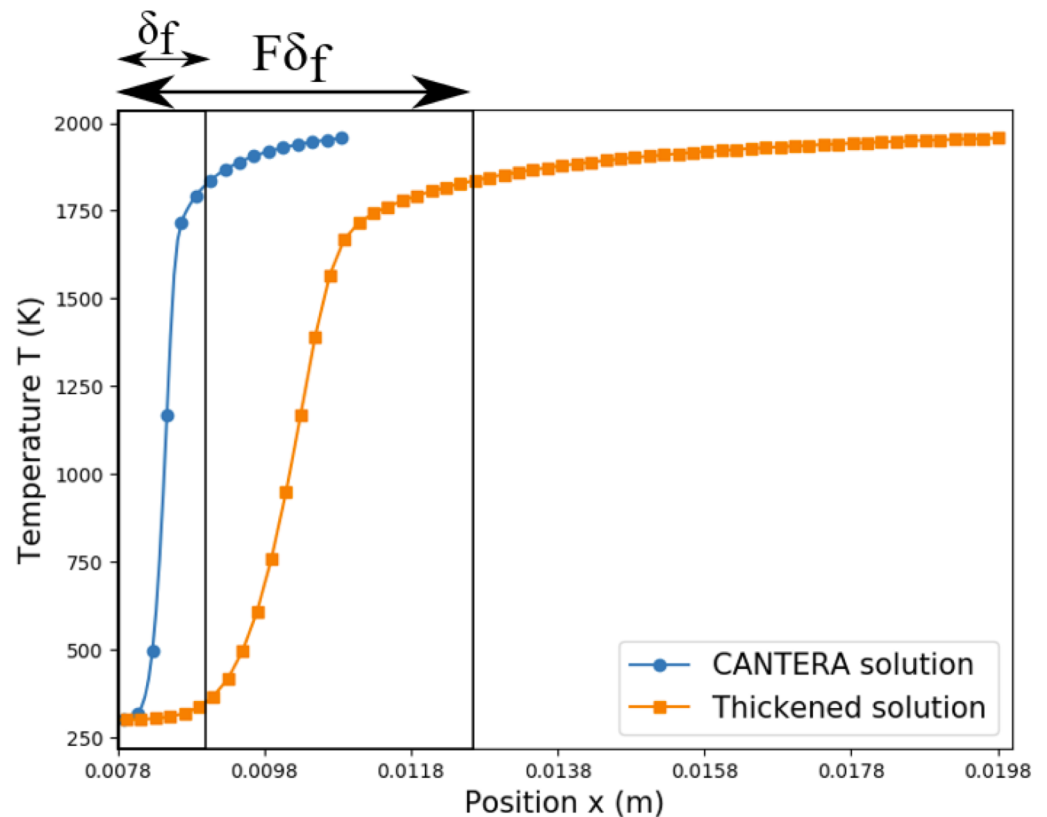
To be able to test the chemistry for

`f.flame.thick = value`

$$\dot{\omega}_k \rightarrow \dot{\omega}_k / F$$

$$D_k \rightarrow D_k F$$

$$S_L \rightarrow S_L$$



[https://cerfacs.fr/chemistry-repo/pub/cantera\\_jypnb/Thickening.html](https://cerfacs.fr/chemistry-repo/pub/cantera_jypnb/Thickening.html)



## 4. Alternative remeshing

Three options for “refine\_grid” parameter:

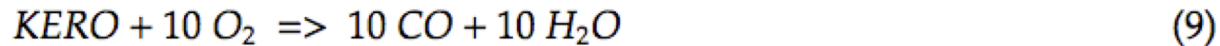
- “**disabled**” : no refinement. Can be useful if one wants to test a regular-spaced grid.
- “**refine**” : default refinement method of CANTERA. Is very useful to refine more the flamefront than the edges.
- “**remesh**” : CERFACS method, useful to go from one grid to another.

```
refine_grid = 'remesh'  
f.solve(loglevel, refine_grid)
```

## 5. *Partial Equilibrium Assumption (PEA)*

- Special to BFER -> correction for the rich part.
- Only available with AVBP format.

The 2S\_KERO\_BFER scheme is based on the two following reactions:



where the forward reaction rates for reactions (9) and (10) are written as:

$$k_{f,1} = A_1 f_1(\phi) e^{(-E_{a,1}/RT)} [\text{KERO}]^{n_{\text{KERO}}} [\text{O}_2]^{n_{\text{O}_2,1}}, \quad (11)$$

$$k_{f,2} = A_2 f_2(\phi) e^{(-E_{a,2}/RT)} [\text{CO}]^{n_{\text{CO}}} [\text{O}_2]^{n_{\text{O}_2,2}}, \quad (12)$$

[https://cerfacs.fr/chemistry-repo/pub/cantera\\_jypnb/Pea.html](https://cerfacs.fr/chemistry-repo/pub/cantera_jypnb/Pea.html)



## 6. *Flamelet computation*

Mixture fraction variable :  $z$

Trick : change of space from  
 **$x$  (position)** to  **$z$  (mixture fraction)**

Faster computations (20s instead of 200s).

Better stability (CDF is very capricious).

No return possible to  $x$ -space.

```
f = ct.Flamelet()
```

[https://cerfacs.fr/chemistry-repo/pub/cantera\\_jypnb/CDF-Flamelet.html](https://cerfacs.fr/chemistry-repo/pub/cantera_jypnb/CDF-Flamelet.html)



## 7. Soot equation

- Enables the computation of soot after a flame in cantera

$$\frac{\partial n}{\partial t} + \underbrace{\nabla \cdot (\mathbf{u}n)}_{\text{Convection}} - \underbrace{\nabla \cdot \left( C_{th} \nu \frac{\nabla T}{T} n \right)}_{\text{Thermophoresis}} = \underbrace{\nabla \cdot (D_s \nabla n)}_{\text{Diffusion}} + \underbrace{\dot{n}_s}_{\text{Source}} \quad (1)$$

[https://cerfacs.fr/chemistry-repo/priv/cantera\\_soot/Handbook\\_cantera-soot.pdf](https://cerfacs.fr/chemistry-repo/priv/cantera_soot/Handbook_cantera-soot.pdf)



## *Bonus: Cantera as an input of AVBP*

- It is possible to generate a 1D flame from Cantera and make an initialization for AVBP

```
f.write_AVBP('name_of_file.csv')
```

- It is possible to generate a *gas\_out* with the help of Cantera.
- It is possible to use Cantera to calculate evaporation with *evol\_evap0D*.
- It is possible to create the *mixture\_database.dat* with the *xml2av* tool.



## *Bonus 2: Cantera as an input of AVBP*

- You have a separate git called cantera-tools
  - Initialize 3D AVBP calculations with cantera
  - Optimize Schmidt & Prandtl numbers

<https://chemistry.cerfacs.fr/en/avbp/avbp-tools-for-chemistry/>





# *BACKUP*

<http://www.cmap.polytechnique.fr/~giovangi/convergent.pdf>

<https://chemistry.cerfacs.fr/en/cantera/cantera-tutorials/>